

# CFD Modelling of an 850 kW Injection Furnace to Investigate NOx Emissions

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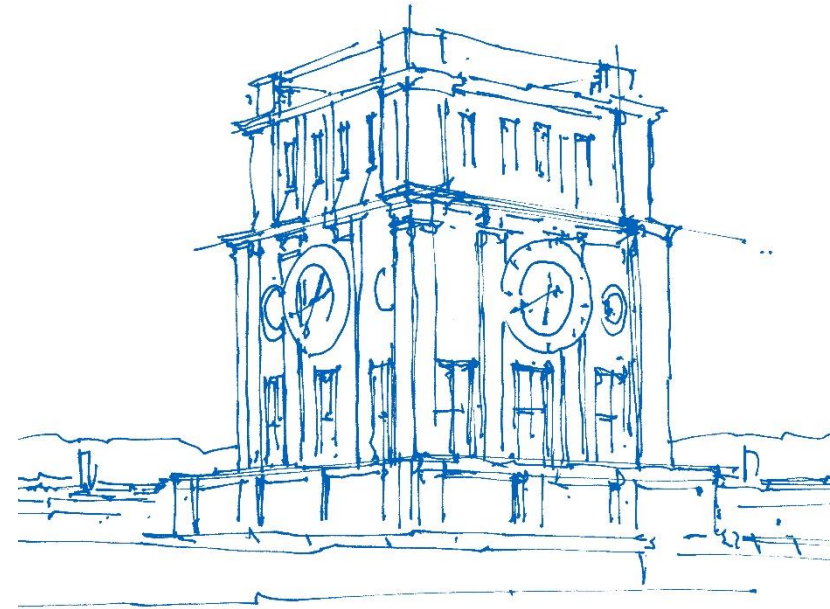
April 4<sup>th</sup>, 2024



Federal Ministry  
of Food  
and Agriculture








Fachagentur Nachwachsende Rohstoffe e.V.



Uhrenturm der TUM

# Agenda

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- Motivation
- 
- Project OptiNOx
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- CFD-Model
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- Scale-Up and Results for the 850 kW Furnace
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- Summary and Outlook



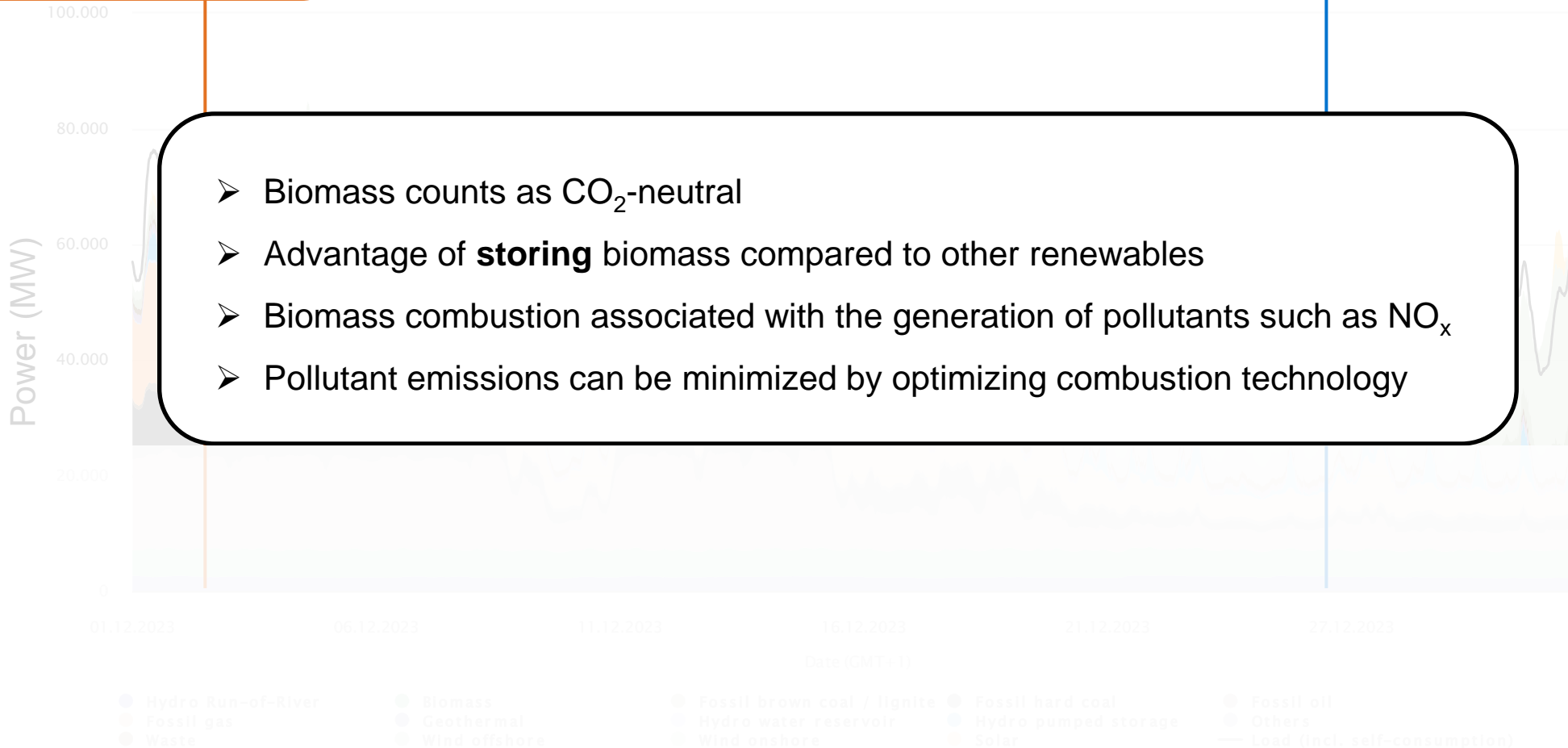
02.12.2023:

- Fossil Fuels: ~ 76 %
- Solar & Wind: ~ 5 %
- **Biomass: ~ 8%**

26.12.2023:

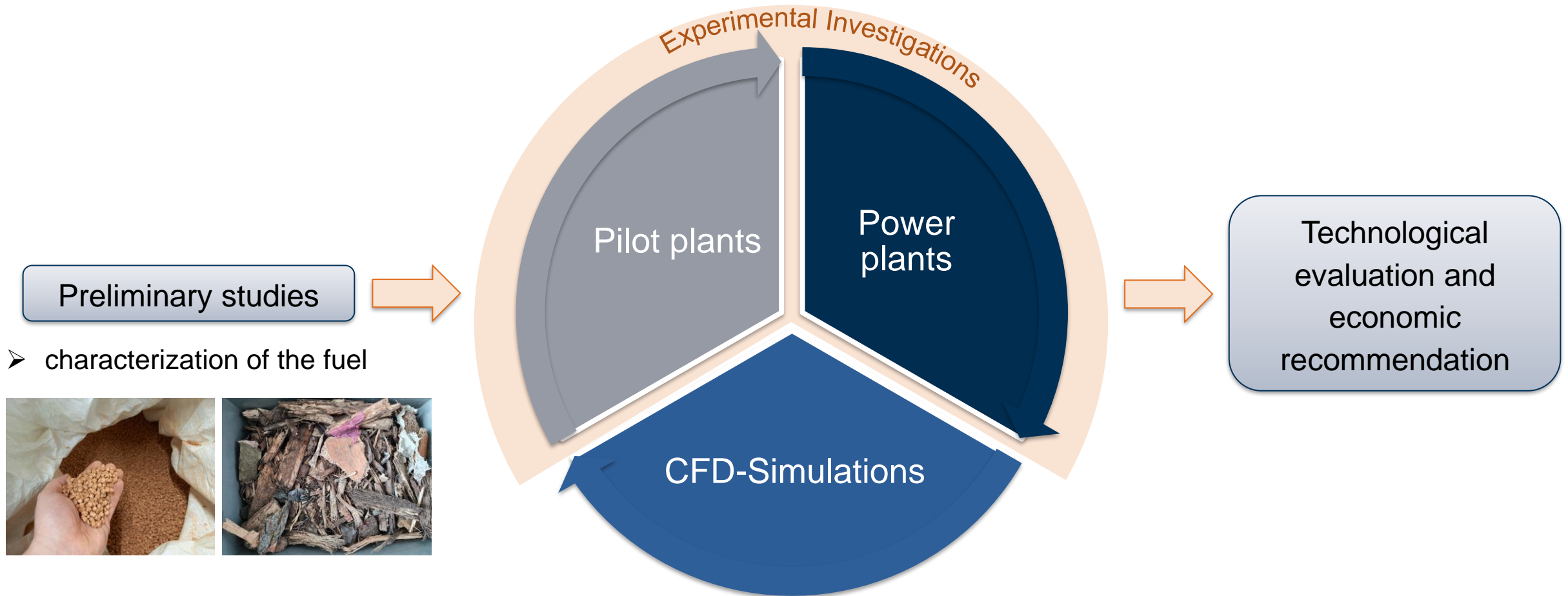
- Fossil Fuels: ~ 14 %
- Solar & Wind: ~ 64 %
- **Biomass: ~ 7%**

Total net electricity generation in Germany in December 2023  
Energetically corrected values



- Biomass counts as CO<sub>2</sub>-neutral
- Advantage of **storing** biomass compared to other renewables
- Biomass combustion associated with the generation of pollutants such as NO<sub>x</sub>
- Pollutant emissions can be minimized by optimizing combustion technology

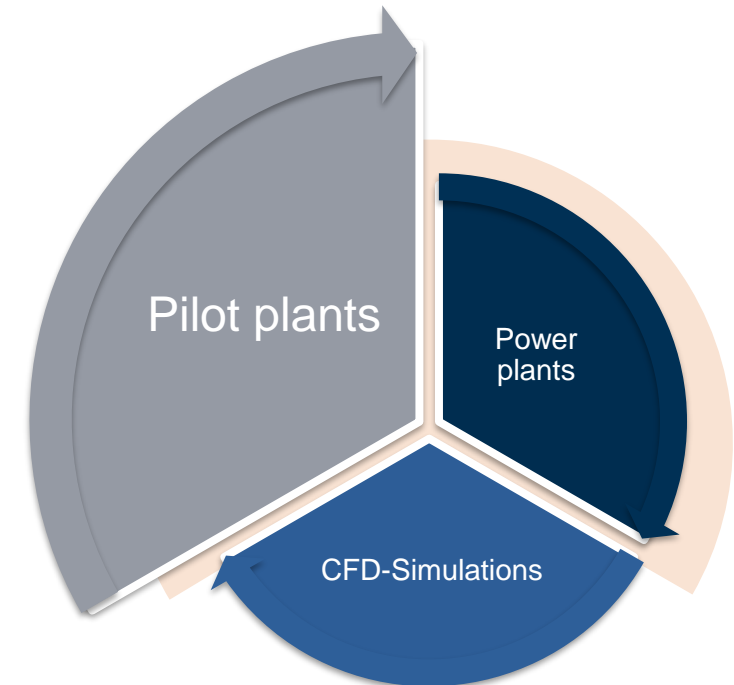
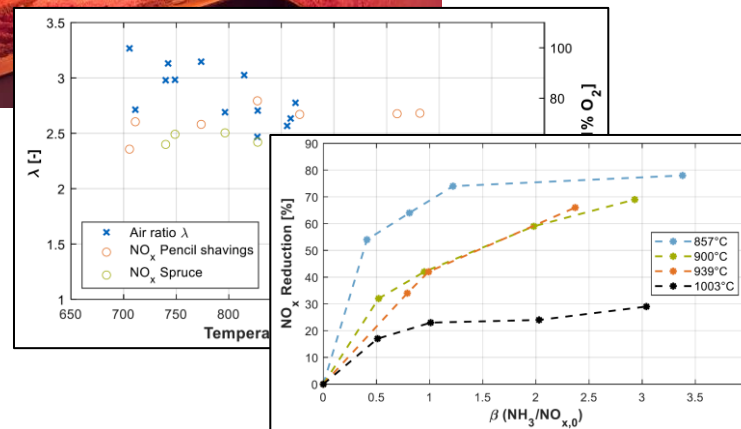
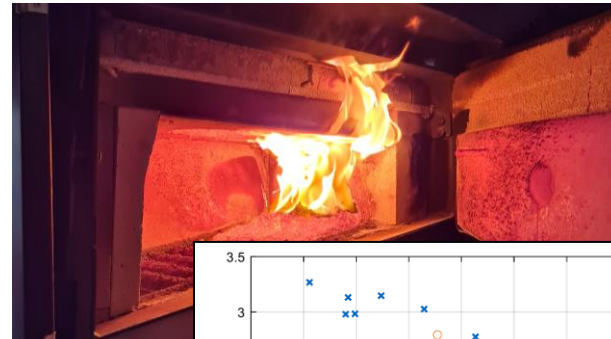
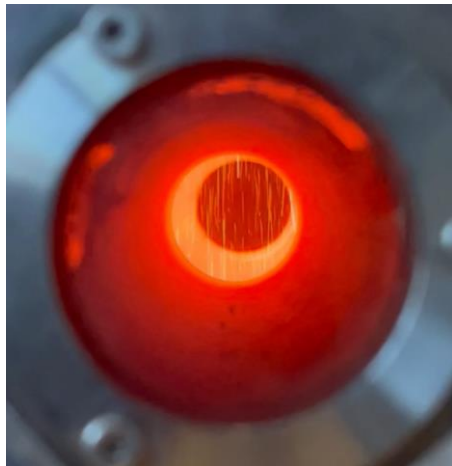
# OptiNOx (Optimization of biomass furnaces with the aim of reducing NO<sub>x</sub> emissions)



# OptiNOx

Pilot plants:

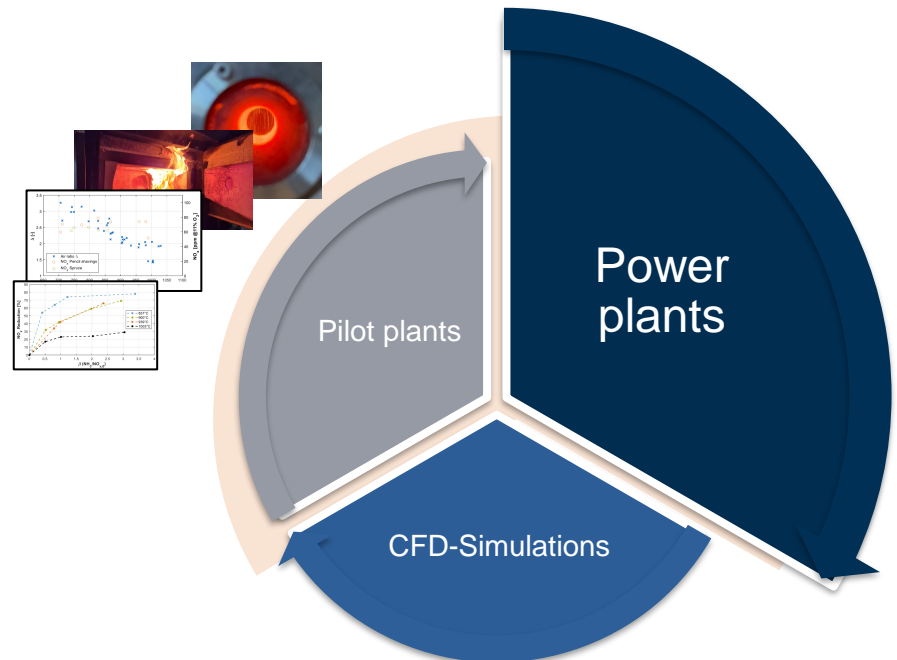
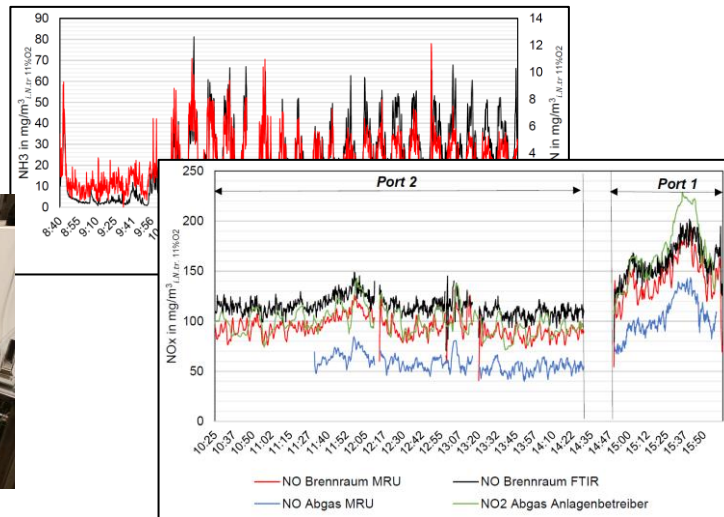
- Combustion of fuel in different pilot-scale plants
- Measurement of NO<sub>x</sub> precursor species (NH<sub>3</sub>, HCN)
- Investigation of primary and secondary measures to reduce emissions



# OptiNOx

## Power Plants:

- Measurements of NO<sub>x</sub> precursor species at different power plants
  - Skærbæk Power Plant (vibrating grate, 154 MW)
  - Avedøre Unit 2 (Straw Boiler) (vibrating grate, 105 MW)
  - Altenstadt HKW (fluidized bed, 49 MW)
  - Staedtler Residue Pencil Wood (injection furnace, 850 kW)

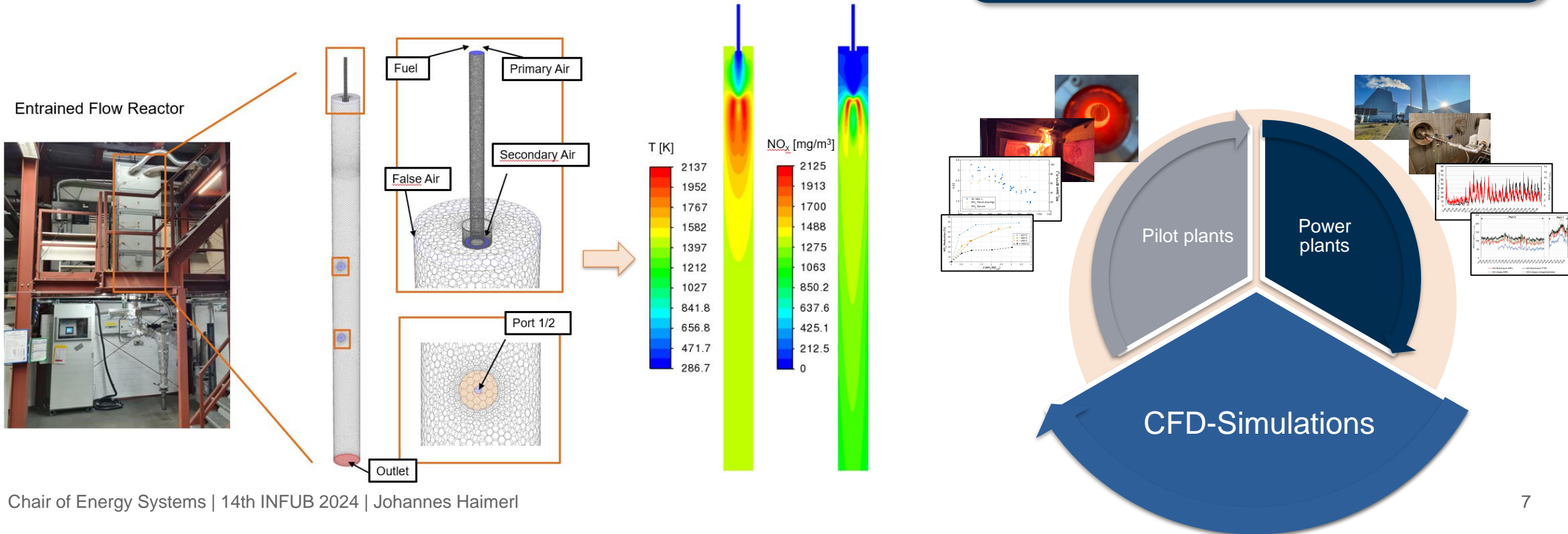


# OptiNOx

## CFD-Simulations:

- Development of NO<sub>x</sub> and burnout models
- Simulation of pilot plants → Validation with the gained experimental data

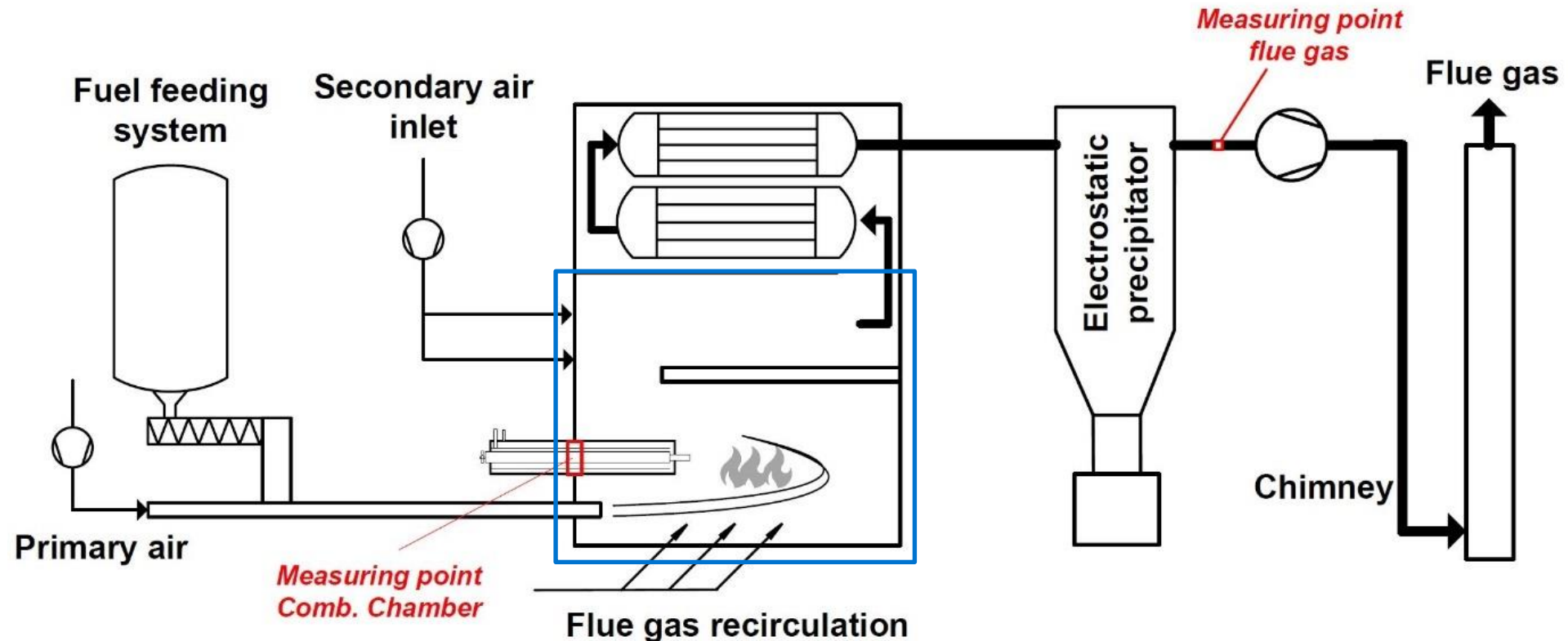
**Scale-Up and Optimization of the power plants**



# Staedtler – 850 kW Injection Furnace

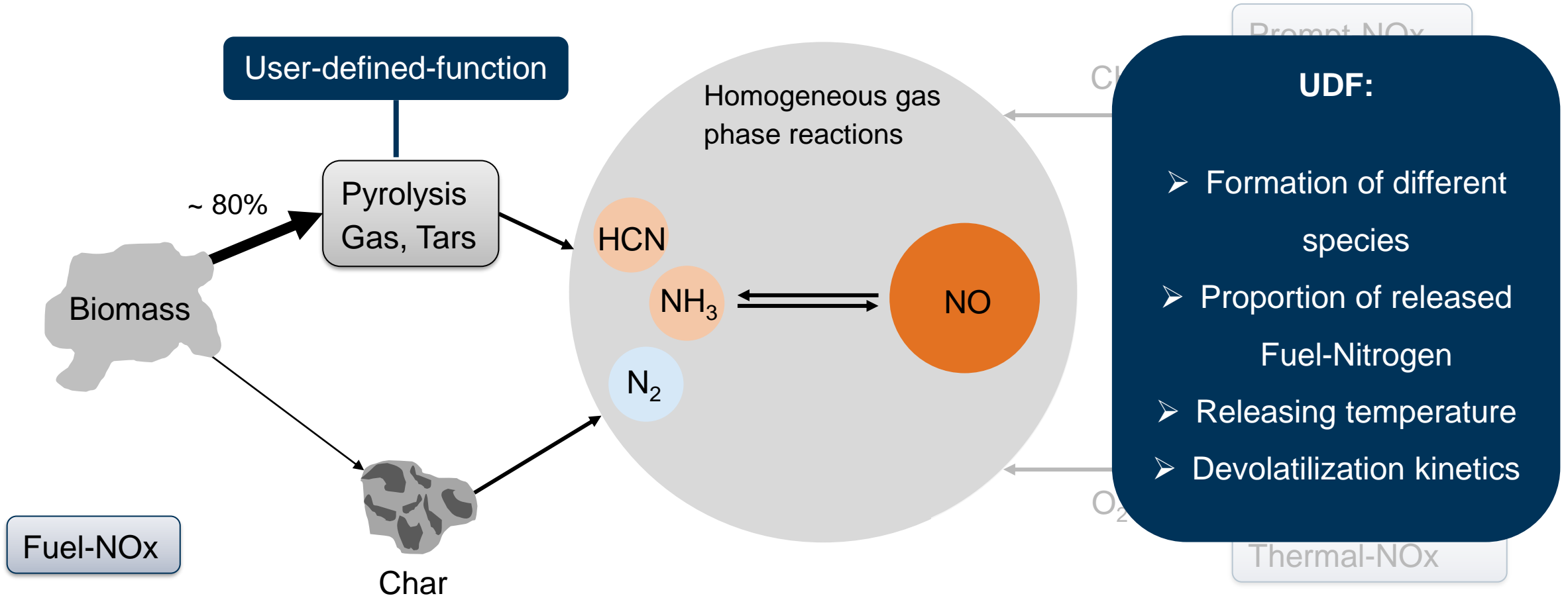
- Combustion of wood residues from pencil production
- Air-Staging and Flue gas recirculation for control of emissions
- Two-point measurement has been conducted

C	52.14	wt.-%
H	5.52	wt.-%
O	33.66	wt.-%
N	0.94	wt.-%
S	0.44	wt.-%
<b>v</b>	<b>79.79</b>	<b>wt.-%</b>
a	0.33	wt.-%
f	6.44	wt.-%
HHV	20.35	MJ/kg





# CFD-Model – NOx formation





# Model – NO<sub>x</sub> Simulation

## Combustion Simulation:

- Energy equation
- Turbulence Model (*realizable k-ε Model; Standard Wall Functions*)
- Radiation Model (*Discrete Ordinates*)
- Particle Tracking (*Discrete Phase Model; Discrete Random Walk Model*)
- Reaction Model (*Eddy Dissipation Concept; ISAT*)



## Pollutant Simulation:

- Fixed temperature and velocity field
- Reaction Model (*Eddy Dissipation Concept; ISAT*)

**Global Reaction Mechanism:** 10 species and 4 reactions

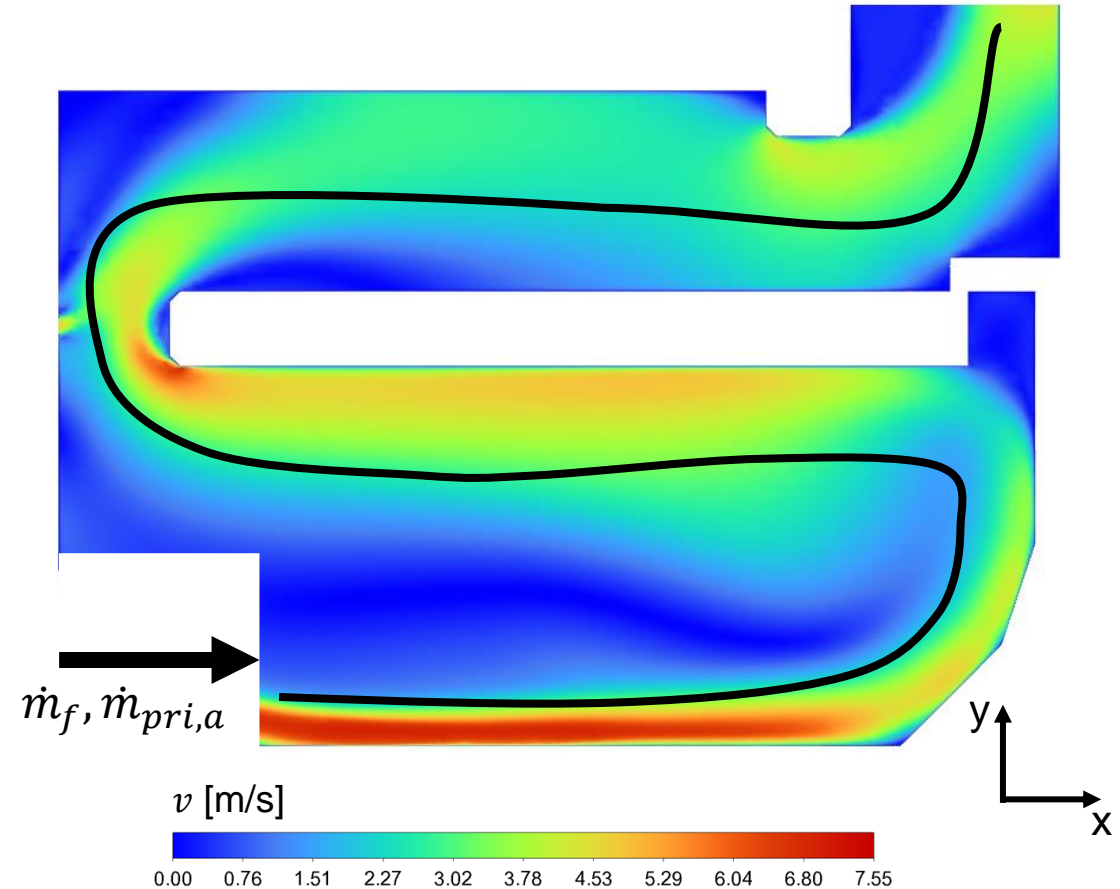
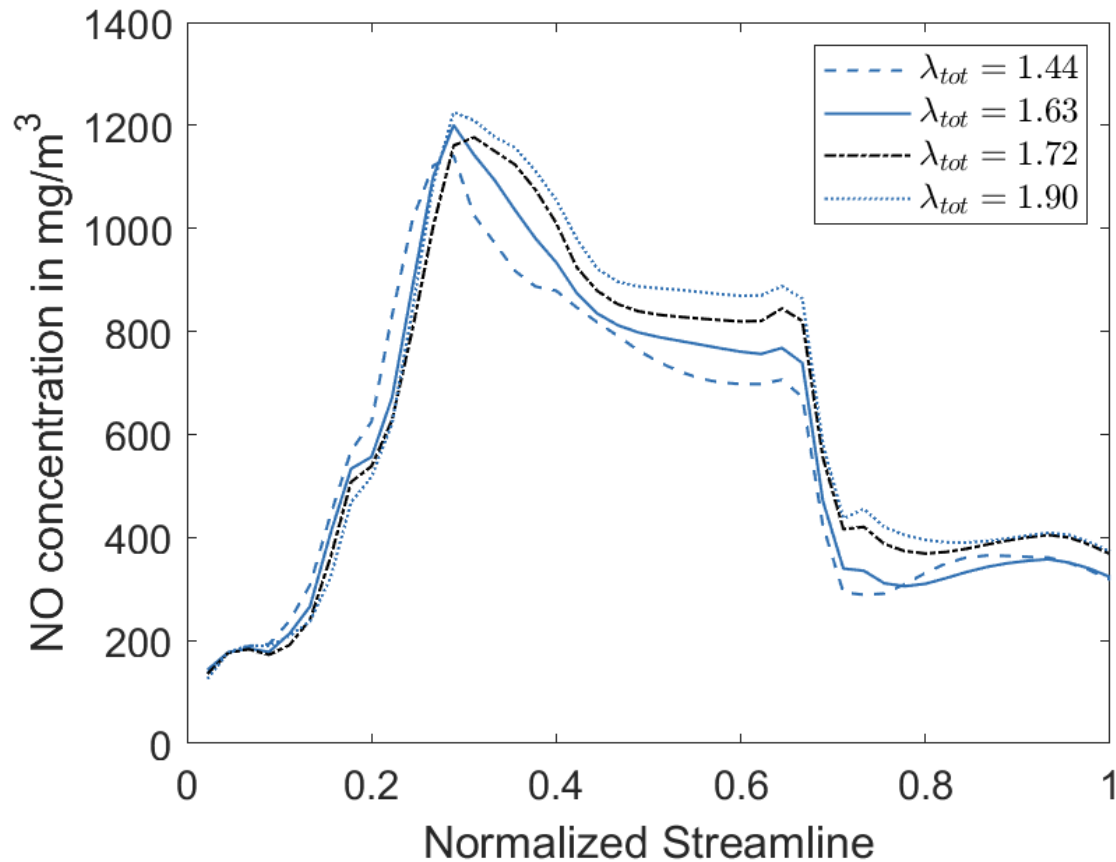
**Skeletal NO<sub>x</sub> Mechanism:** 38 species and 168 reactions

Mesh independence study (850.000 cells)



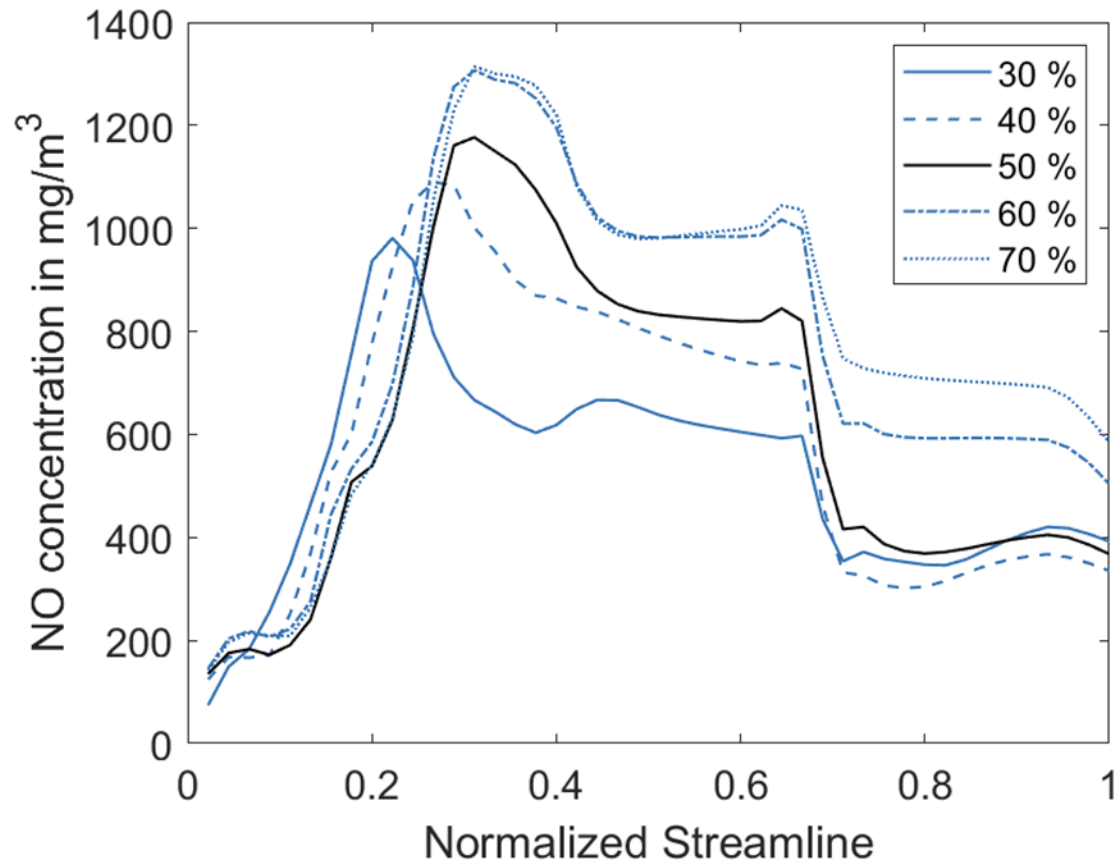
# Influence of Fuel-Air Ratio

Fixed ratio of primary to secondary air (50:50)

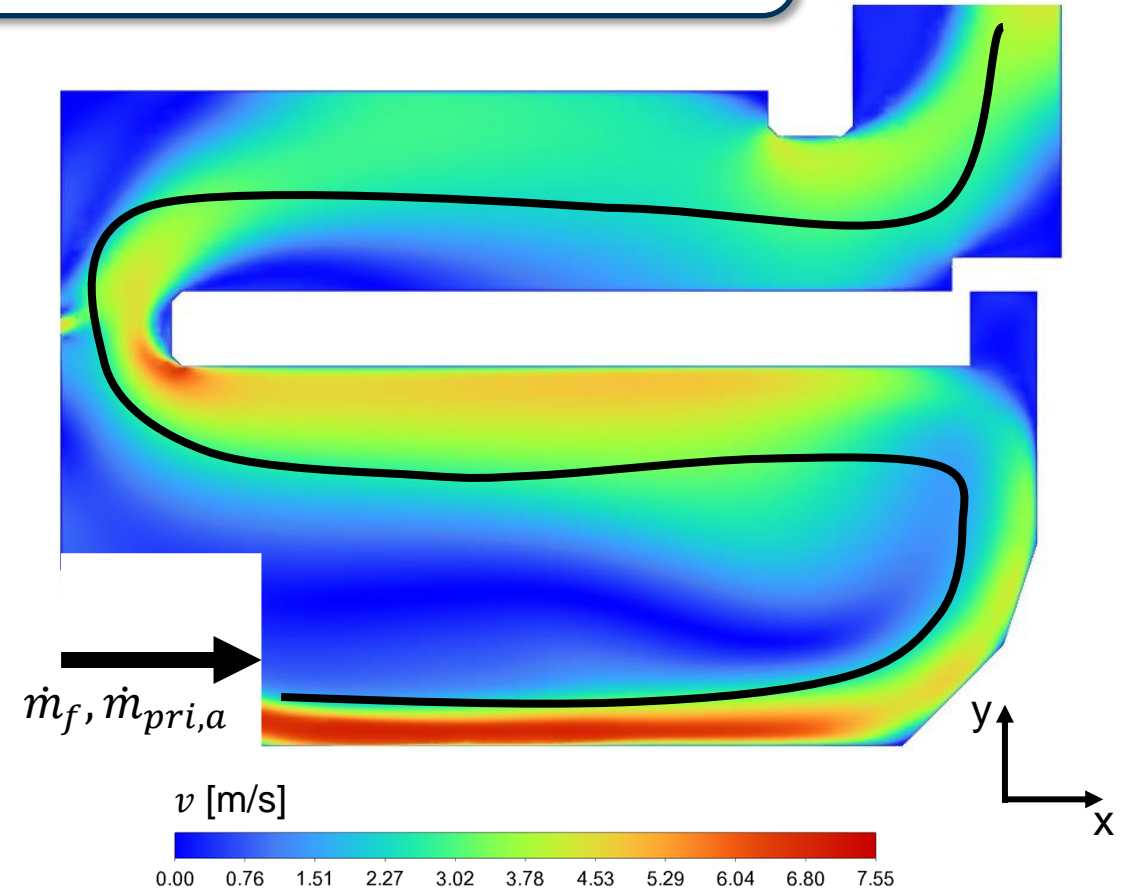


# Influence of Air Staging

Fixed Fuel-Air Ratio with  $\lambda_{tot} = 1.7$



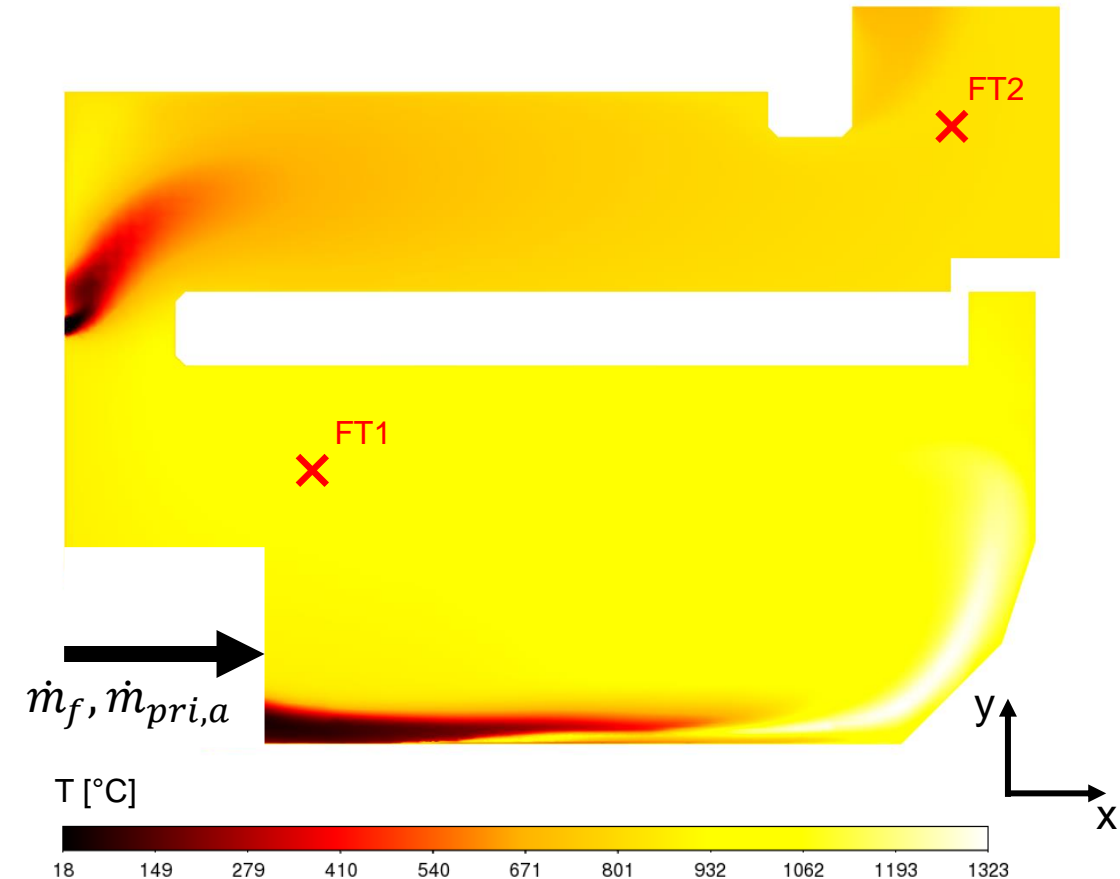
**Optimal Ratio:**  
40% primary air to 60% secondary air



# Scale-Up – Staedtler – 850 kW Injection Furnace

Fuel: Wood shavings from pencil production (N-Fraction: 0.94 wt.%)

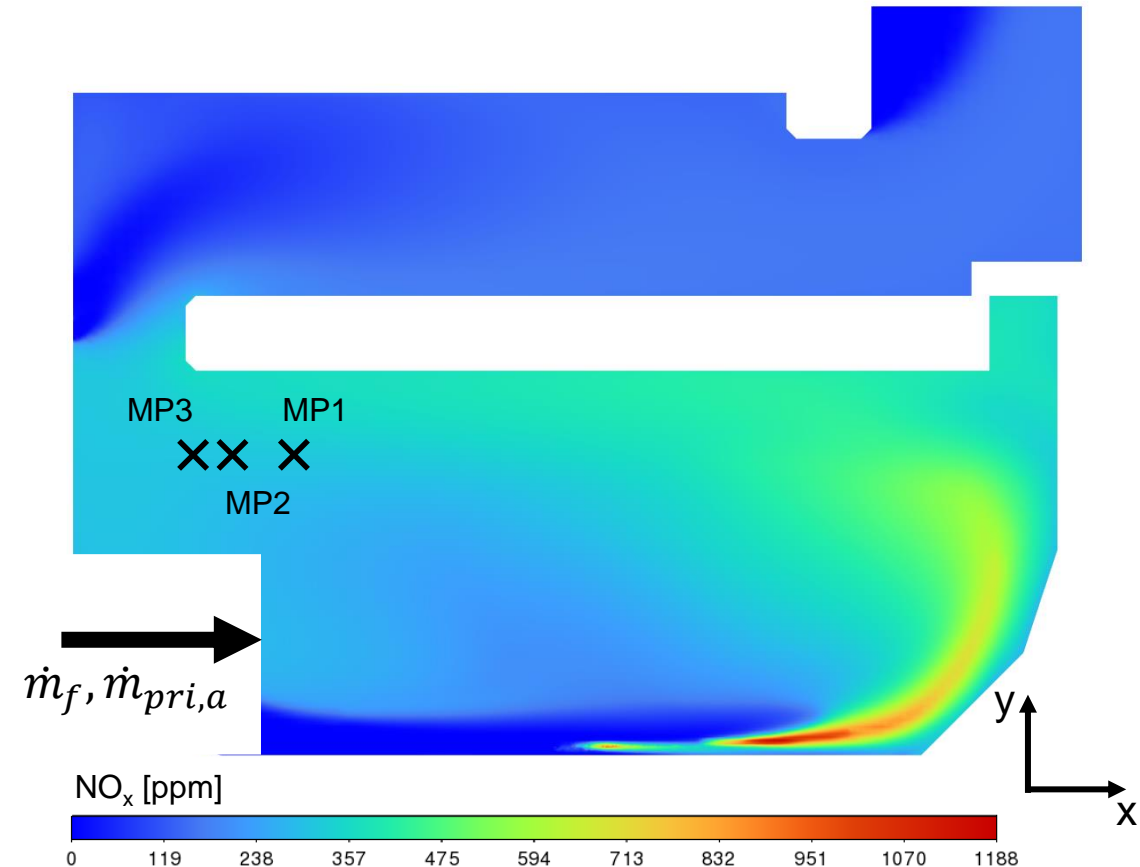
	Measurement	Simulation
<b>Outlet</b>		
CO <sub>2</sub> [%]	12.36	11.59
O <sub>2</sub> [%]	5.01	5.74
CO [ppm]	648.98	489.58
NO [mg/m <sup>3</sup> @6%O <sub>2</sub> ]	<b>127.01</b>	<b>278.94</b>
<b>Temperature</b>		
FT1 [°C]	1060.01	954.14
FT2 [°C]	892.75	831.26



# Scale-Up – Staedtler – 850 kW Injection Furnace

Fuel: Wood shavings from pencil production (N-Fraction: 0.94 wt.%)

	Measurement	Simulation
<b>MP1 (60cm)</b>		
NO [ppm]	102.26	259.71
NH <sub>3</sub> [ppm]	70.88	159.73
HCN [ppm]	6.78	73.19
<b>MP3 (30cm)</b>		
NO [ppm]	92.43	265.87
NH <sub>3</sub> [ppm]	72.16	221.18
HCN [ppm]	5.26	97.86





# Outlook

## Comparison

- Model can be scaled up and used for modelling of injection furnaces
- Influence of Fuel-Air Ratio as well as Air-Staging was analyzed
  - Optimal Air-Staging Ratio could be identified

## Next Steps:

- Compare with trends from new measurements at the power plant
- Include release of char-N and  $\text{NO}_x$  formation due to secondary tar cracking reactions
- Implement variable releasing temperatures for the species

# Thank you for your attention!

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