



Flexible power and synthesis plant concepts with integrated chemical power storage

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Structure

- **Project HotVeGas**
- **Future challenges for conventional power plants**
- **Power-to-Gas Technology**
- **Analysis of IGCC-EPI concept**
- **Conclusion**

Research Project Overview HotVeGas II – Future high temperature gasification and gas cleaning processes



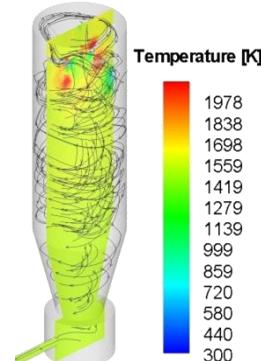







Gasification Kinetics

- Kinetics at high temperature (1800° C) and high pressure (50 bar)
- Development of reaction models for heterogeneous char gasification

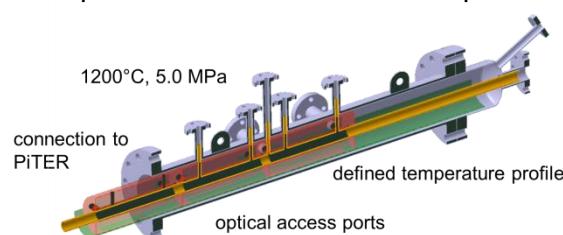


CFD - Modeling

- Design of pyrolysis and gasification models
- Particle tracking and slag flow modeling
- Modeling of condensation of trace elements

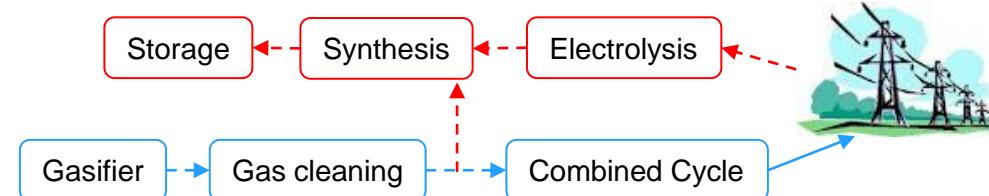
Cooling Behavior of Trace Elements

- Condensation behaviour of trace elements
- Deposition of trace elements on probes



Overall Process Evaluation

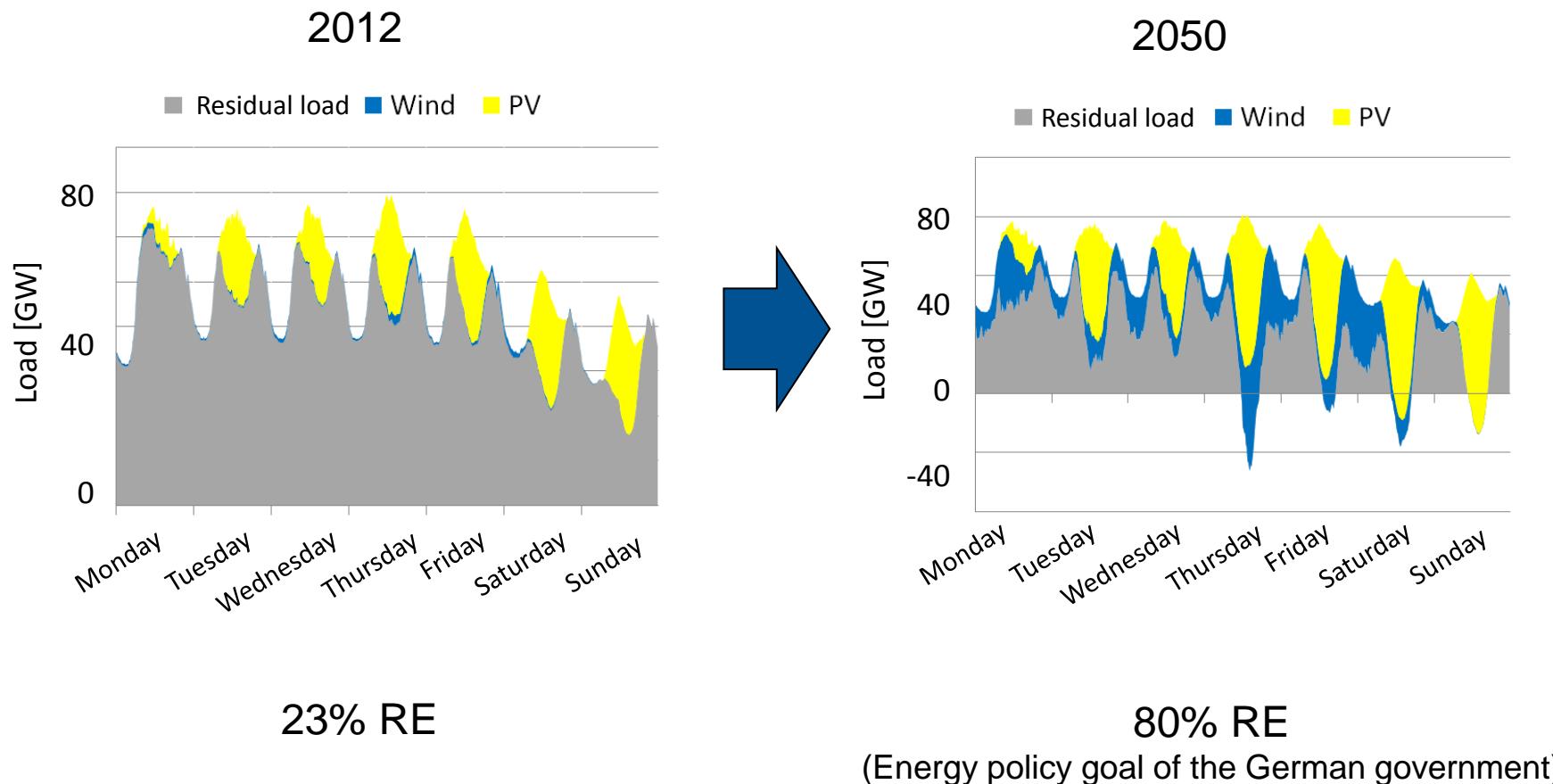
- Flexible IGCC-concepts with polygeneration and excess energy storage
- Biomass co-gasification
- Potential of future technologies



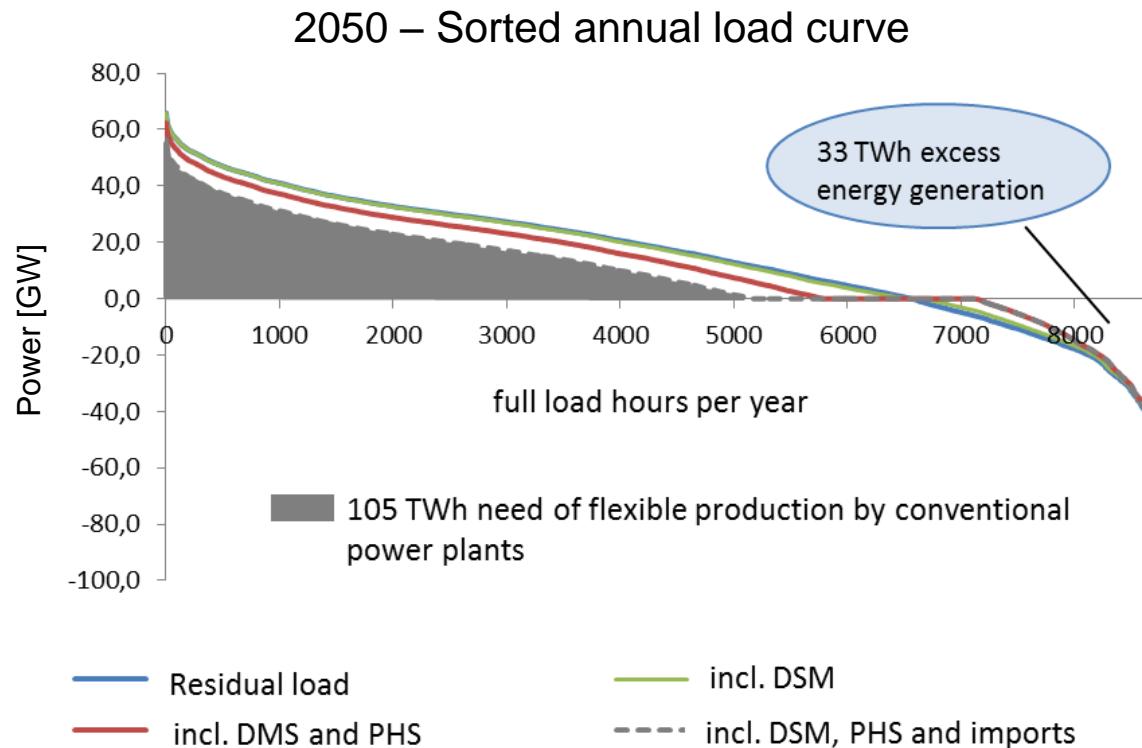
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Future development of energy system in Germany



Future challenges for conventional power plants



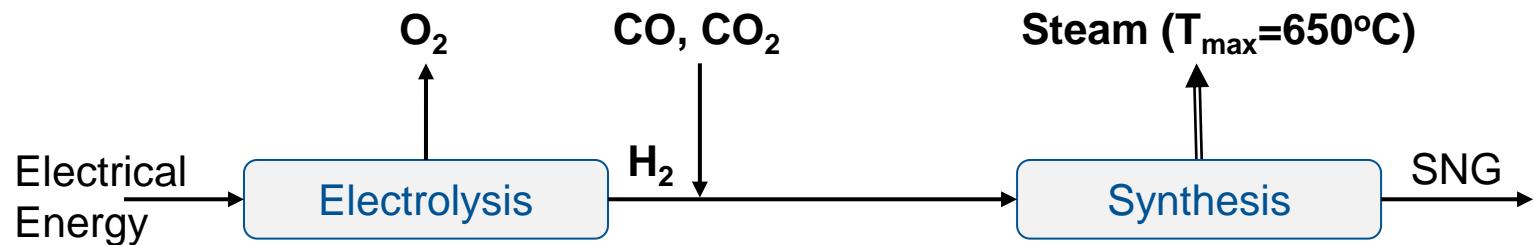
Challenges:

- Decreased utilization
- Increased flexibility requirement
- Excess energy storage

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Power to gas technology



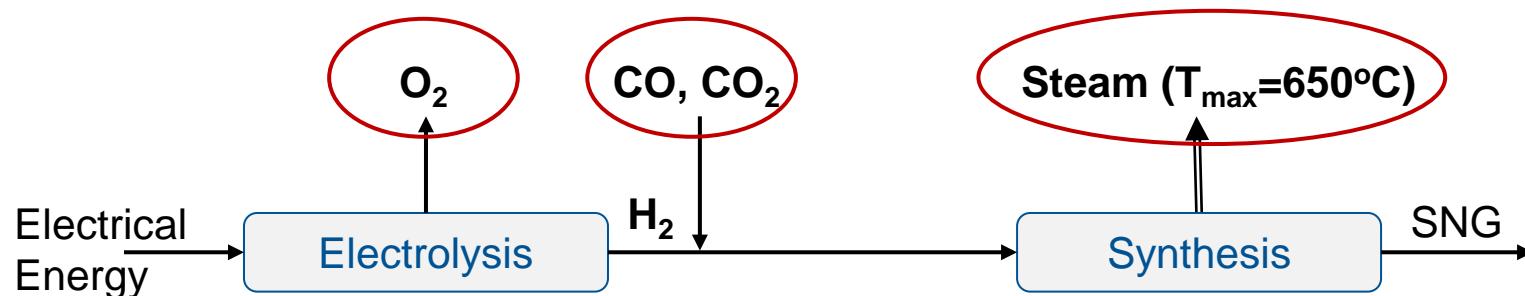
Advantages

- + High energy density
- + Full use of the existing NG infrastructure
- + Reconversion with state of the art technology possible

Disadvantages

- High costs
- Low power-to-power efficiency

Motivation for system integration concepts



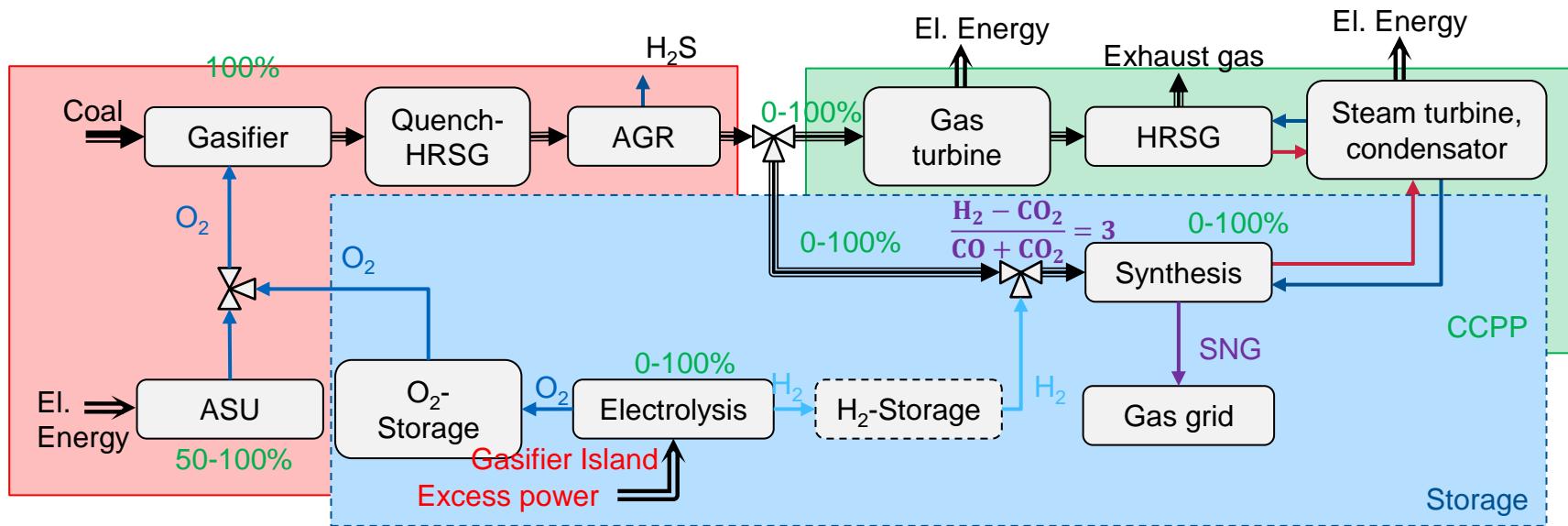
Overall efficiency of P2G:

$$\eta_{\text{Power} \rightarrow \text{Power}} = \eta_{\text{Electrolysis}} \times \eta_{\text{CO}_2} \times \eta_{\text{SNG}} \times \eta_{\text{CC}} = 0,7 \times 0,95 \times 0,8 \times 0,6 = 32 \%$$

Possibilities for efficiency enhancement:

- Use of the byproduct O₂ of the electrolysis
- Integration of the CO/CO₂ source
- Use of the heat of the exothermal synthesis
- CHP plant for reconversion of the SNG

IGCC-EPI (Excess Power Integration) concept



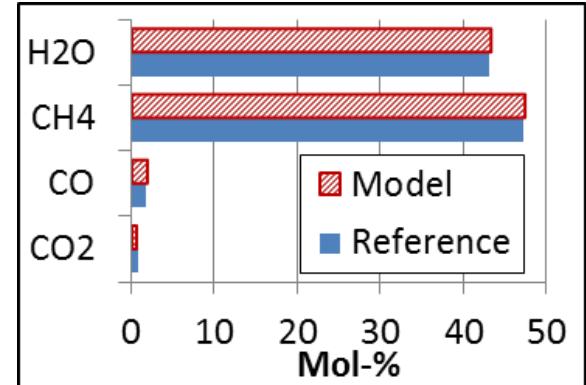
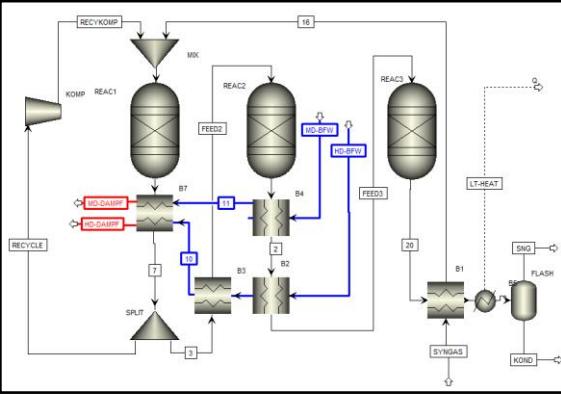
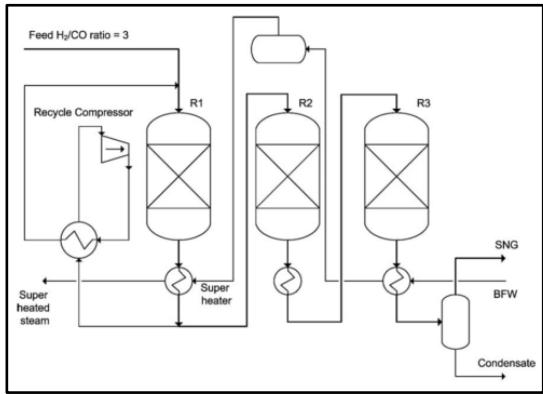
Features:

- + High **positive and negative flexibility** at baseload operation of the gasifier island
- + **No CO-Shift reactor and CO_2 sequestration** for adjustment of synthesis gas composition → conversion losses and investment costs can be avoided
- + **Integration of O_2** from electrolysis for gasification
- + **Integration of the heat** of the synthesis plant in the CCPP

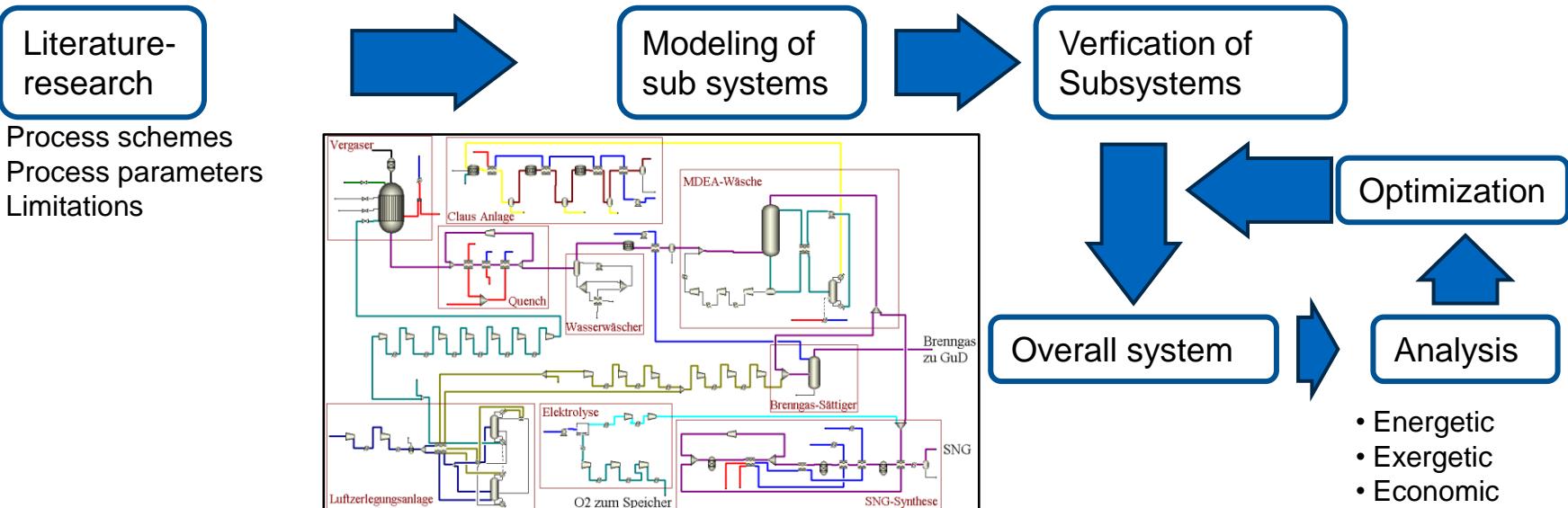
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Methodology – Overall System Evaluation



Reference: Industrial data from a 20 MW TREMP process



Main boundary conditions of the simulation of a 125 MW_{th} concept

Storage properties:

SNG feed in pressure:

$$p_{SNG} = 60 \text{ bar}$$

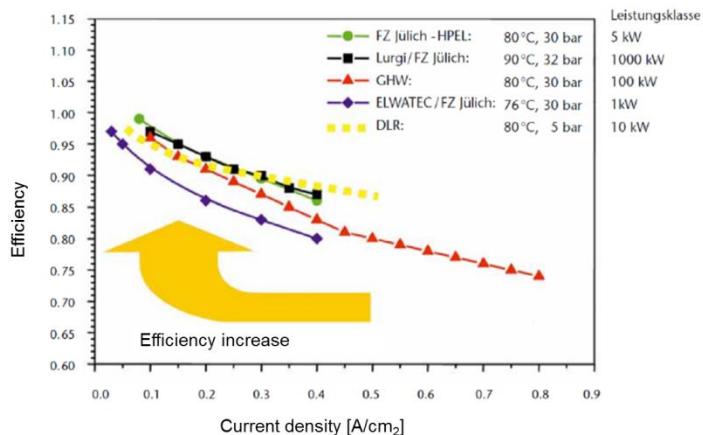
Mean O₂ storage pressure:

$$p_{O_2} = 75 \text{ bar}$$

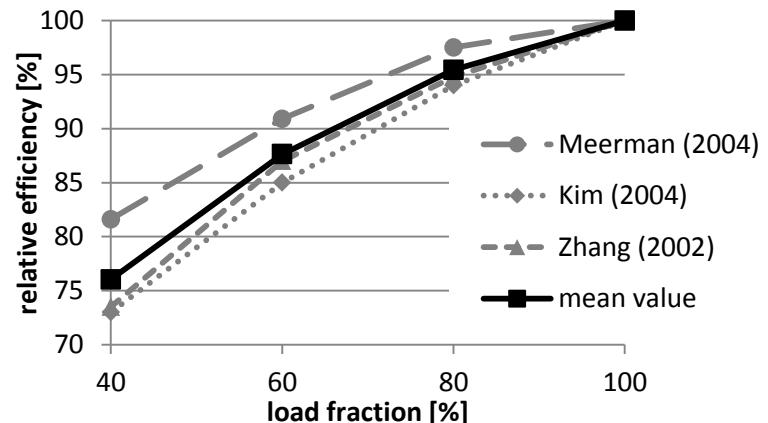
Specific energy consumption of the electrolyzer: $E_{S,\text{Elektrolyse}} = 4,4 \text{ kWh/Nm}^3$ (400 mA/cm²)

Part load behavior:

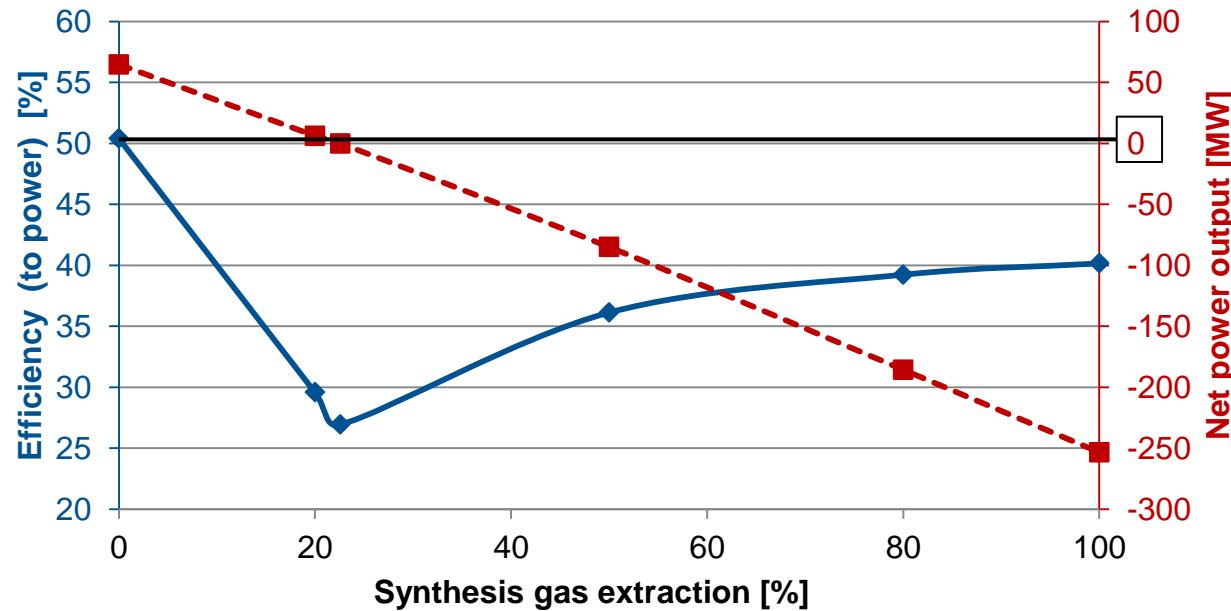
Electrolysis



Gas turbine



Overall system part-load efficiency (including reconversion of storage medias to power)



Efficiency definition:

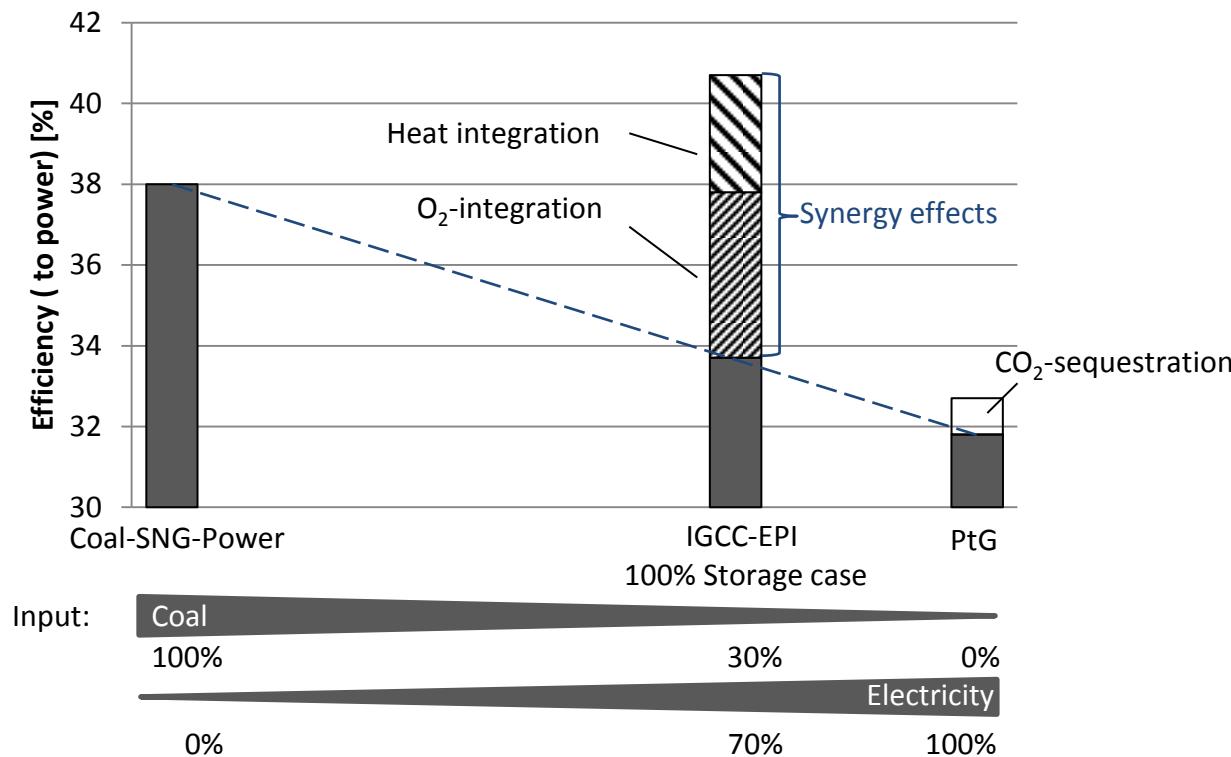
$$\eta_{\text{Power/coal} \rightarrow \text{power}} = \frac{\frac{P_{el}(SNG)}{\dot{m}_{SNG} \cdot H_{u,SNG} \cdot \eta_{GUD} + \dot{m}_{O_2} (LZA_{Aq} + w_{s,V})} + P_{Netto}(P_{Netto} > 0)}{\frac{P_{el}(O_2)}{\dot{m}_{SK} \cdot H_{u,SK}} - P_{Netto}(P_{Netto} < 0)}$$

$\underbrace{\hspace{10em}}$ $\underbrace{\hspace{10em}}$

$$Q_b(SK)$$

$$\eta_{GUD} = 60\%; \quad LZA_{Aq} = 0,27 \text{ kWh/kg}$$

Impact of synergies on overall storage efficiency



→ Synergy effects result in an overall efficiency advantage of 6.4% points

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Conclusion

- Increased flexibility requirements for future conventional power plants
- High excess power potential and need for long-term energy storages
- Combination of power-to-gas and gasification technology results in:
 - Superior operation range of conventional power plant
 - High overall storage efficiency due to synergy effects



Thank you for your kind attention.

Questions???